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### Carbon capture and utilization

### HIGHLIGHTS

**Processes and technology status** – Carbon dioxide (CO<sub>2</sub>) capture, storage, and utilization (CCS and CCU) are effective technologies for CO<sub>2</sub> fixation <sup>1</sup>. CCU is about the reusing of the captured CO<sub>2</sub> by utilizing it directly or as a feedstock for the production of valuable products <sup>2</sup>.

**Cost** - The cost of CCS/CCU depends mainly on the CO<sub>2</sub> source and purity. The scale of CO<sub>2</sub>, the implemented capturing technology, and CO<sub>2</sub> taxes are significant factors of CCS/CCU costs <sup>3</sup>. The specific capital costs per ton of captured CO<sub>2</sub> by 2025 are estimated to be  $20-40 \in_{2013} {}^4$ .

**Potential and barriers** – CCS/CCU technologies are at a good advanced status concerning its design and optimization at a significant rate over the past years and are a potential solution to the problems of greenhouse-gas emissions <sup>3</sup>. The most threatening risks are the high costs and a lack of supporting regulation <sup>5</sup>.

**Carbon capture and utilization** – Carbon capture, storage, and utilization or separation (CCS/U) aim to reduce global anthropogenic CO<sub>2</sub> emissions to tackle climate change by capturing carbon at the emission source and preventing its entry into the atmosphere. In parallel, some studies deal with the capturing of CO<sub>2</sub> from

**Process overview** –  $CO_2$  capture is accomplished by employing several methods like the use of membranes, chemical looping, cryogenic distillation, etc. <sup>3</sup>. The collected  $CO_2$  can be stored in geological sites or can be utilized for enhanced oil recovery or in chemical industries. The  $CO_2$  utilization techniques are young and significant research is needed to make these processes economically viable <sup>7</sup>.

**Carbon capture technologies and methods** – Different capture and separation technologies via several methodologies exist, and their costs depend on the CO<sub>2</sub> amount, CO<sub>2</sub> partial pressure, and the concentrations of contaminations such as  $N_2$ <sup>5</sup>, <sup>8</sup>.

the ambient air  $^3$ .



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Capture technologies typically are categorized as pre-combustion, oxy-fuel combustion, and post-combustion processes <sup>5</sup>. Figure 1 depicts a schematic overview of the different CO<sub>2</sub> capture categories <sup>5</sup>. Among CCS technologies, post-combustion is the most mature alternative to capture  $CO_2$  and finds use to retrofit existing carbon emissions <sup>9</sup>. Postand pre-combustion captures rely on methodologies that can separate CO<sub>2</sub> from the mixed stream, via i) Solvent scrubbing, ii) Solid adsorbent, iii) Adsorption, iv) Membrane, v) Cryogenic distillation<sup>3</sup>.

### Carbon utilization pathways - CO<sub>2</sub>

utilization is the process of using emitted carbon dioxide ( $CO_2$ ) as a raw material or as a catalyst for new products. Possible carbon utilization pathways include the usage of  $CO_2$  in the manufacturing of fertilizers, urea, methanol, oil and gas recovery in addition to water desalination projects and electrochemical conversion to certain chemicals <sup>3</sup>.

Conversion of CO<sub>2</sub> to synthetic fuels was identified as a promising pathway to scaling up the carbon capture technologies, as the valuable products would offset the carbon capture and conversion costs <sup>6</sup>. Other ways of reducing carbon emissions include negative emission techniques, renewable resources, and direct air capture techniques. CO<sub>2</sub> utilization is possible via both direct and indirect pathways <sup>3</sup>. As figure 2 depicts, methanol is the most prevalent product of CO<sub>2</sub> conversion as reported in the literature set, followed by CO<sub>2</sub>-based chemicals and fuels <sup>2</sup>.

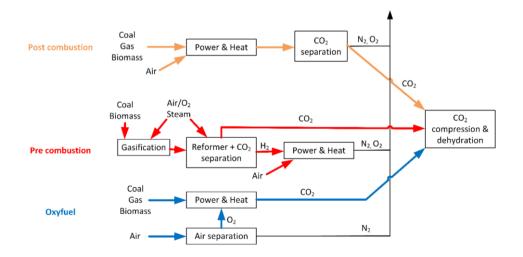


Figure 1: Overview of CO<sub>2</sub> capture technologies <sup>5</sup>.



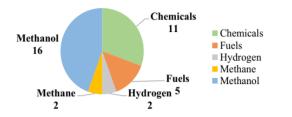


Figure 2. CO<sub>2</sub>-derived product categories addressed in the literature set <sup>2</sup>

Moreover, green methanol production, based on intermittent renewable energy sources, requires a more flexible operation mode and close integration with other sections, such as the electrical grid and electrolysis processes <sup>10</sup>.

### CCS and CCU in Belgium -

ArcelorMittal Belgium has started the construction of two new groundbreaking facilities at the Ghent site to reduce carbon emissions. The two installations represent a total investment of 160 million euros and will avoid approximately 400,000 tons of  $CO_2$  emissions per year in the first phase <sup>11</sup>.

Moreover, The Power to Methanol project in Antwerp will produce methanol from captured  $CO_2$  combined with hydrogen that has been sustainably generated from renewable electricity <sup>12</sup>.

## Investment and production costs –

CO<sub>2</sub> is not available cost-free and requires

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financial investments for capturing, purification, and transportation depending on the site location. Some studies state that the capture cost amounts to 70-80% of the total cost of a full CCS system <sup>5</sup>. The most important drivers of CCS cost are the economics of scale, partial pressure of  $CO_2$ , energy costs, and technology innovation. By increasing the storage size and the  $CO_2$ patricidal pressure, CCS costs decrease <sup>13</sup>. Overall, high purity sources include ethylene oxide (EO) and ammonia plants. For example, the potential of CCS in the EO plants in the Dutch industry is abating  $\sim 0.1$ Mt<sub>CO2</sub> at an abatement cost of  $\sim 25 \notin_{2013}/t_{CO2}$ <sup>4</sup>. Prefabricated, modular carbon capture reduce technology can capital and operational costs by up to 75% and 50%, respectively <sup>14</sup>. In general, CCS costs may vary widely on a case-by-case basis <sup>15</sup>. Costs in natural gas processing, fertilizer, and bio-ethanol have a relatively narrow band of variance across all countries, with a range of 17.7 – 23.9  $€_{2017}^{1}$  per ton of avoided CO<sub>2</sub>. Details of CCSU costs are available in the table 1.

**Energy requirements** – The physical solvent-based processes require less energy compared to the chemical absorption processes. Energy demands of physical

<sup>&</sup>lt;sup>1</sup> 20  $\$_{2017}$  to 27  $\$_{2017}$ , 1  $€_{2017} = 1.13$   $\$_{2017}^{20}$ 

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solvent-based processes range between 160 and 180 kWh per ton  $CO_2$  recovered.

For the production of chemicals, the  $CO_2$ reacts with organic compounds to form carbonates/carbamates via the carboxylation process. Although the conventional processes are broadly used the CO<sub>2</sub> reaction with organic substances gives better fixation with fewer energy requirements <sup>7</sup>.

### Potential for CCS deployment -

World-wide the highest potential and market size for  $CO_2$  utilization are in the chemical and oil industry, with the Enhanced Oil/Gas Recovery (EOR/EGR) and to have the greatest potential for non-captive demand, the urea production, the polymer processing as well as in fuel and chemical synthesis such as renewable methanol, formic acid. It is also important that the cement sector has a great uptake potential whereas in the food sector, also a medium potential exists (e.g. carbonation, packaging, and horticulture) <sup>16</sup>. Currently,

there are eighteen large-scale facilities in operation in the world, five under construction, and twenty in various stages of development  $^{17}$ .

### **Recent innovations on CCS/CCU**

The recent innovation on carbon capture is the modular CycloneCC which works with patented APBS solvents<sup>2</sup> to achieve a 50% operating cost reduction <sup>19</sup>. CycloneCC is based on a novel process technology called rotating packed beds (RPBs) as shown in figure 3. The flue gas is introduced to the RPB from the outer edge of the packing and exits at the inner edge where the solvent enters. Therefore, the gas and the liquid contact each other in a counter-current fashion. The flue gas is absorbed by the solvent and the  $CO_2$  present selectively reacts with the active components in the solvent thereby temporarily locking the  $CO_2$  within the solvent <sup>19</sup>. The mission of CycloneCC is to achieve 25.8 €2021 <sup>3</sup> cost of carbon capture especially for the hard-toabate industries <sup>19</sup>.

<sup>&</sup>lt;sup>2</sup> APBS-CDRMax® is a commercially-available CO<sub>2</sub> capture solvent used for industrial flue gases or off-gases with CO<sub>2</sub> concentrations ranging from 3-25% by volume.

<sup>&</sup>lt;sup>3</sup> 30 \$2021; 1 \$2021, Oct. =  $0.86 \text{ EUR}_{2021, Oct.}$ (average)



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Figure 3. CycloneCC unit structure

Moreover, CycloneCC technology offers a smaller size which is 10 times smaller than the conventional CO<sub>2</sub> capturing unit. When commercialized, industrial companies and

customers will be able to install these units in less than 8 weeks highly improving their operational profile and any downtime our customers may face <sup>19</sup>.

Table 1. Summary table of CCS costs

Plant	Cost *
EO	25 €2013/tco2
Natural gas and bio-ethanol processing,	17.7 – 23.9 €2017/tco2
Cement	$92 - 171.7 \notin_{2017} / / t_{CO2}$
Iron and steel	62.8 - 105.3 € <sub>2017</sub> /t <sub>CO2</sub>
Coal-fired power plants	34 - 68 € <sub>2018</sub> /t <sub>CO2</sub>
Direct Air Capture	200 - 1000 € <sub>2018</sub> /t <sub>CO2</sub>
Large CO <sub>2</sub> exhaust sources	18 - 90 € <sub>2015</sub> /t <sub>CO2</sub>
High purity CO <sub>2</sub> sources	5.4 – 10.8 €2015/tco2
Price of green hydrogen	2.6 - 3.8 €2018/kgH2
Coal-based CO <sub>2</sub> catalytic hydrogenation	2500-3300 €2020/tProduced petrochemicals
CO <sub>2</sub> transport and storage	10 € <sub>2017</sub> /t <sub>CO2</sub> **
Offshore transport and storage	14.2 - 32.7 €2017/tco2
CO <sub>2</sub> storage costs in liquid form	4.46 - 13.86 €2018/tco2
Truck transportation of the CO <sub>2</sub>	0.22 € <sub>2018</sub> /t <sub>CO2</sub> per km

\* Costs depend on the type of capturing. For example, the pre-combustion route could offer a cheaper cost than that of post-combustion and oxy-fuel combustion routes by 38–45 and 21–24%, respectively (in theory).

\*\* Increasing the annual transport flow rate from 0.5 to 5 Mt<sub>CO2</sub>/y would reduce average transport cost more than three times, from over 20  $\epsilon_{2017/t_{CO2}}$  to around 6  $\epsilon_{2017/t_{CO2}}$ . Moreover, the cost of CO<sub>2</sub> storage contributes relatively small amounts to overall project costs.

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